

Introduction

Recent advances in biologics development are primarily focussed on development of high titre producing cell lines to substantiate the requirement of high dosage mAbs which may be as high as 600-700 mg drug per dose. This also brings in the requirement of subcutaneous injectables to alleviate the hassles of IV infusion. Therefore, to achieve both these objectives, substantial work has also been initiated for development of high concentration formulation along with high titre cell lines.

One of the biggest challenges for the development of high concentration formulation is increase in viscosity which impact the injection force and patient comfort. As part of purification process flow, the concentration of the protein molecules is achieved by TFF unit operation which is also the unit operation where this challenge is encountered the most. This poster focuses on the strategy to mitigate this challenges and achieve a concentration of >200 mg/mL for mAbs as well as other mammalian recombinant proteins.

Barriers during TFF

<h3>Viscosity Increase</h3> <ul style="list-style-type: none"> Indicators – ΔP increase 	<h3>Pressure Limitations</h3> <ul style="list-style-type: none"> Higher pressure can lead to process disruption 	<h3>Scalability challenge</h3> <ul style="list-style-type: none"> Non linear changes in flow dynamics during scale up
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Key contributors

Protein-protein interaction	Module resistance	Suboptimal TMP or Cross flow rate
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Levers optimized and Indicators

Operational Parameters	<ul style="list-style-type: none"> TMP and CFR optimization Protein Recovery Strategy
Composition of load and diafiltration buffer	<ul style="list-style-type: none"> Viscosity reduction excipients Load conditioning
Membrane selectivity	<ul style="list-style-type: none"> Feed screens Channel configurations

Levers optimized and Indicators

Key Indicators

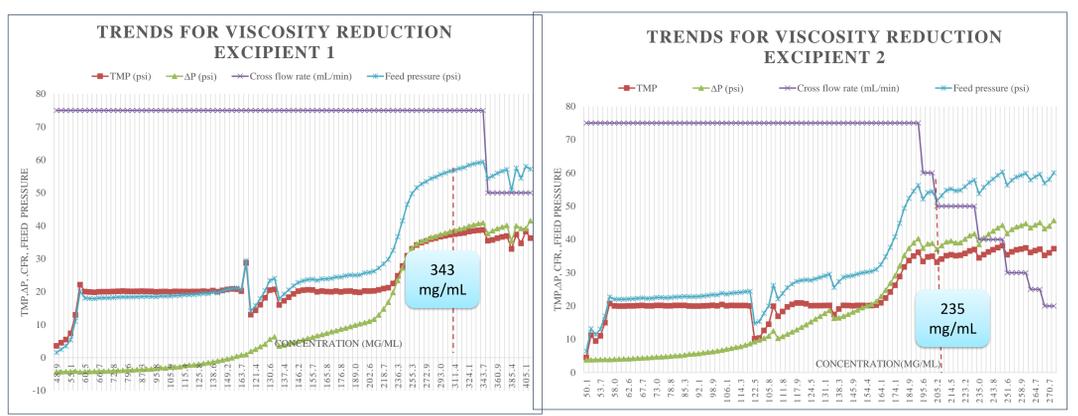
Trend for Differential Pressure (ΔP) (Indicator for viscosity increase)	Retentate Concentration at ΔP_{max}	Recovery %
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Module Resistance

<h3>Type- D screen</h3>	<h3>TangenX EP Screen</h3>
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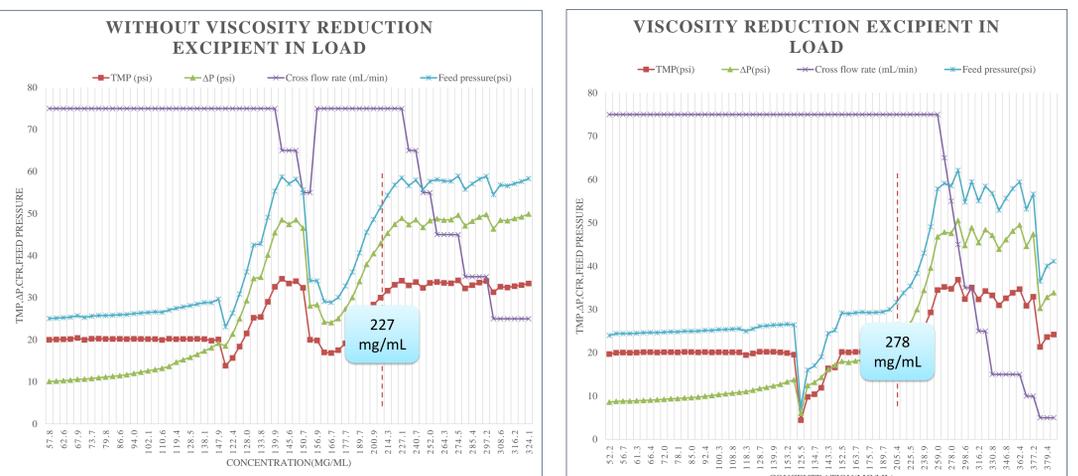
Lower module resistance is observed for TangenX EP screen for which the feed channel configuration supports higher flow rate of >500 LMH. This promotes sweeping phenomenon and prevents protein accumulation

Viscosity reduction excipients



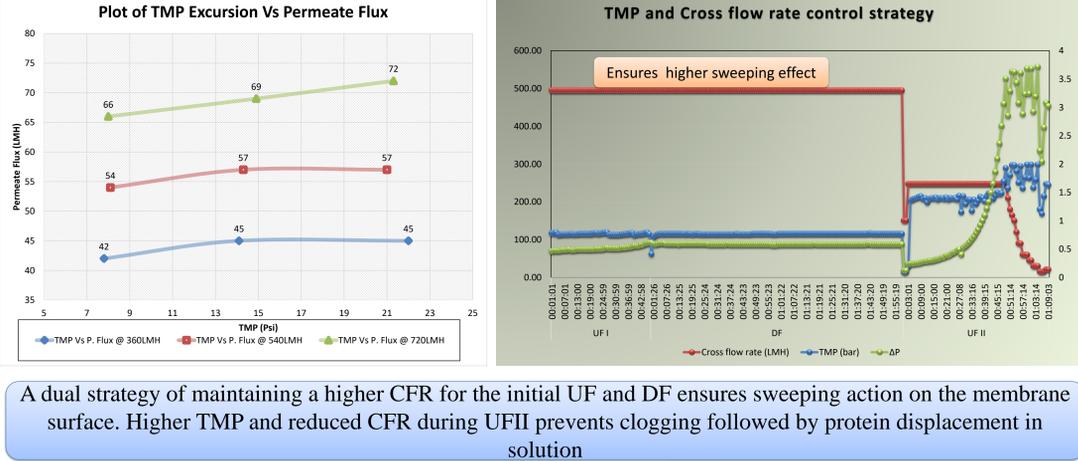
Impact of viscosity reduction excipients were studied with two excipients. It was observed that excipient 1 provided comparatively better control on differential pressure compared to excipient 2

Load conditioning



The delay observed for increase in ΔP after conditioning of the load, is due to impact of the viscosity reduction excipient on reducing the P-P interactions and thus deferring the gel formation.

TMP, Cross flow rate



A dual strategy of maintaining a higher CFR for the initial UF and DF ensures sweeping action on the membrane surface. Higher TMP and reduced CFR during UFII prevents clogging followed by protein displacement in solution

Recovery strategy

Low recovery observed during development and pilot scale. Post optimization during scale up of recovery strategy, protein was efficiently displaced from the surface and an increment of 21% recovery was achieved in Pilot scale run2.

Conclusion

During high-concentration TFF unit operations, pressure drop escalation and gel layer formation on the membrane surface are significant challenges to achieving concentrations >200 mg/mL at the drug substance stage. The strategies discussed in this work effectively mitigate these issues by reducing protein-protein interactions and minimizing gel layer formation on the membrane surface. This results in better displacement and higher recovery during the TFF process. By applying these approaches, consistent concentration >200 mg/mL was successfully achieved at the pilot scale and subsequently scaled up to 2000L at GMP.

*Ragunath, Bala & Wang, Bin & Patnaik, Priyabatra & Janssens, Jeroen. (2012). Best Practices for Optimization and Scale-Up of Microfiltration TFF Processes. Bioprocessing Journal. 11. 30-40. 10.12665/J111.Ragunath.